

# Thermo Midterm 2

## ● Ch. 5 → Control Volumes and Conservation of Mass

### ● Mass and Volume Flow Rates

$$\dot{m} = \rho A v = \rho \dot{V}$$

$\frac{\text{kg}}{\text{s}}$                        $\frac{\text{kg}}{\text{m}^3} \frac{\text{m}^3}{\text{s}}$

● In steady flow, mass flow rate = const

### ● Flow Work and Energy

$$\bullet \quad W_{\text{flow}} = P V ; \quad w_{\text{flow}} = P v$$

●  $\Theta$  = Total energy for flow, per unit mass

$$\bullet \quad \Theta = P v + e = P v + (u + ke + pe)$$

$$\Theta = h + \frac{v^2}{2} + gz$$

$$\bullet \quad \dot{E}_{\text{mass flow}} = \dot{m} \Theta$$

### ● Energy analysis for control volumes

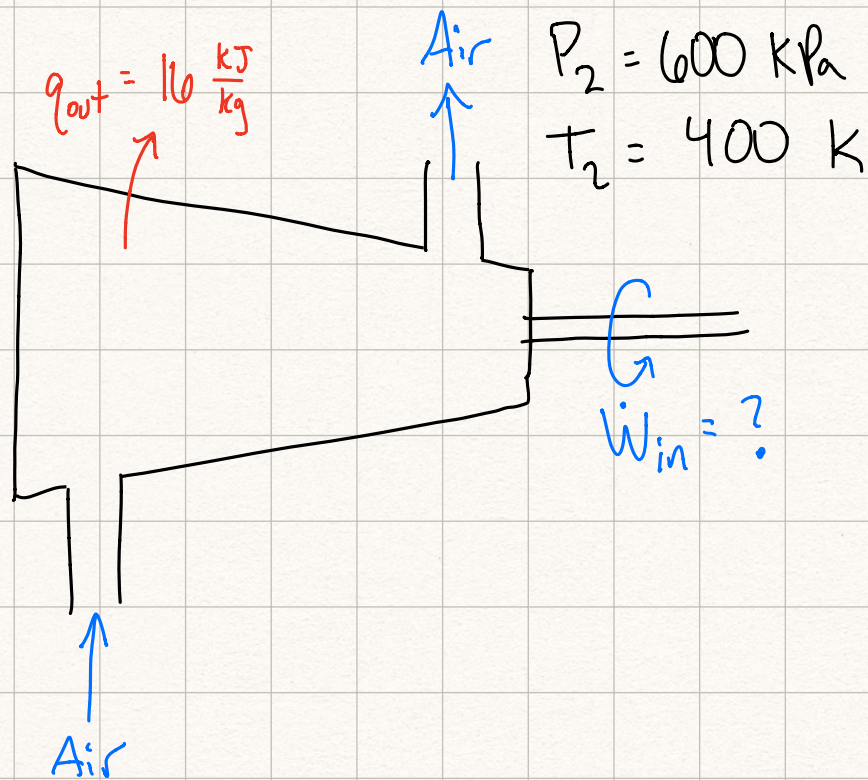


- $E_{in} - E_{out} = \Delta E_{system}$

- $\dot{E}_{in} - \dot{E}_{out} = \frac{d}{dt} (E_{system})$

5-6

Air in a steady compressor



$P_1 = 100 \text{ kPa}$

$T_1 = 280 \text{ K}$

$\dot{m}_1 = 0.02 \frac{kg}{s}$

- $\dot{E}_{in} - \dot{E}_{out} = \frac{d}{dt} (E_{system}) = 0 \text{ (steady)}$

$\dot{E}_{in} = \dot{E}_{out}$



$$\dot{W}_{in} + \dot{E}_{mass\ in} = \dot{Q} + \dot{E}_{mass\ out}$$

$$\dot{W}_{in} = \dot{Q} + \dot{E}_{mass\ out} - \dot{E}_{mass\ in}$$

$$\dot{W}_{in} = \dot{Q} + \dot{m}_{out} \theta_{out} - \dot{m}_{in} \theta_{in}$$

$$\dot{m}_{in} = \dot{m}_{out} = \dot{m}$$

$$\dot{W}_{in} = \dot{Q} + \dot{m} (\theta_{out} - \theta_{in})$$

$$\dot{W}_{in} = \dot{m} q_{out} + \dot{m} (\theta_{out} - \theta_{in})$$

$$\dot{W}_{in} = \dot{m} (q_{out} + \theta_{out} - \theta_{in})$$

$$\dot{W}_{in} = \dot{m} (q_{out} + \cancel{h_{out}} + \cancel{k_{e,out}} + \cancel{p_{out}} - (\cancel{h_{in}} + \cancel{k_{e,in}} + \cancel{p_{in}}))$$

$$\dot{W}_{in} = \dot{m} (q_{out} + h_{out} - h_{in})$$

Table A.17

$$T_{at} \rightarrow h_{at} = 400.98 \frac{\text{kJ}}{\text{kg}}$$

$$T_{in} \rightarrow h_{in} = 280.13 \frac{\text{kJ}}{\text{kg}}$$

$$\dot{W}_{in} = (0.02 \frac{\text{kg}}{\text{s}}) (16 \frac{\text{kJ}}{\text{kg}} + 400.98 \frac{\text{kJ}}{\text{kg}} - 280.13 \frac{\text{kJ}}{\text{kg}})$$

$$\dot{W}_{in} = 2.74 \text{ kW}$$

## Chapter 6 Review

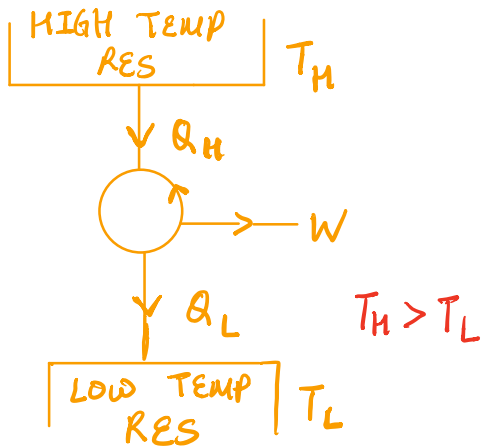
### Second Law of Thermodynamics

#### Limitations of 1st Law of Thermodynamics:

- i] Direction of Heat Transfer
  - ii] Mutual transformation of heat & work
  - iii] The rate of heat transfer
- } 2<sup>nd</sup> Law answers these two.

#### Heat Engine & Refrigerator/Heat Pump

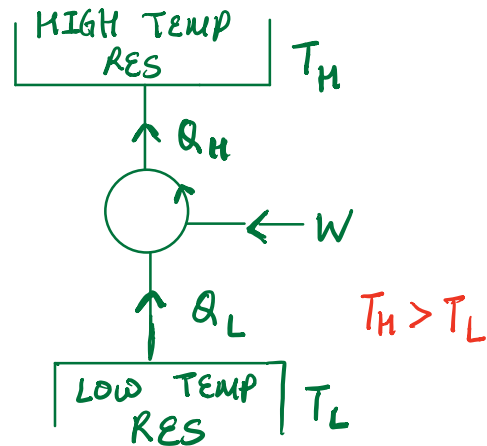
thermal energy to work



$$Q_H = Q_L + W$$

or,  $Q_H - Q_L = W$

eg. internal combustion engine,  
steam power plant



$$Q_H = Q_L + W$$

or,  $Q_H - Q_L = W$

refrigerator  $\Rightarrow$  extract heat from sink  
heat pump  $\Rightarrow$  dump heat to source



Efficiency of heat engine,

$$\eta_{HE} = \frac{W}{Q_H} \frac{[\text{Output}]}{[\text{Input}]}$$

$$= \frac{Q_H - Q_L}{Q_H}$$

$$= 1 - \frac{Q_L}{Q_H}$$

⊗

Coefficient of Performance,

$$COP = \frac{\text{Desired effect produced}}{\text{Energy supplied}}$$

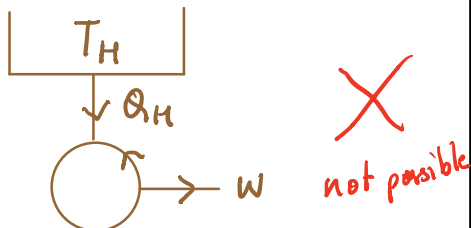
$$COP_R = \frac{Q_L}{W}$$

$$= \frac{Q_L}{Q_H - Q_L}$$

$$COP_{HP} = \frac{Q_H}{W}$$

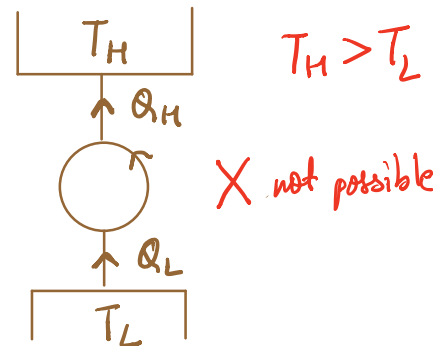
$$= \frac{Q_H}{Q_H - Q_L}$$

It is impossible to construct a heat engine which will operate in a cycle and will transfer heat only with a single reservoir.



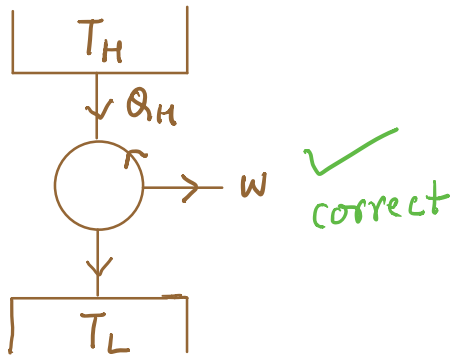
you cannot convert full amount of thermal energy from a reservoir solely into work. You have to deposit into another reservoir

It is impossible to construct a device which will operate in a cycle and will produce no effect other than transfer of heat from a low-temp body to a high-temp one.



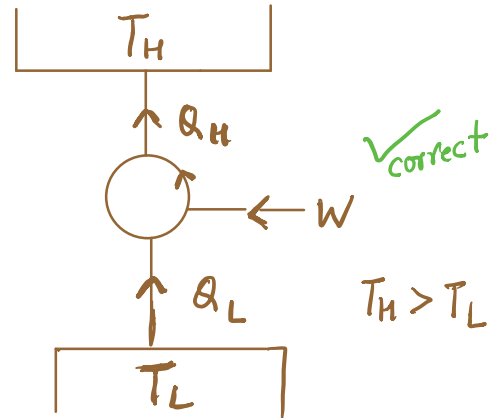
heat will not flow from low temp to high temp, unless & unless you supply external work





$$\eta_{HE} = 1 - \frac{Q_L}{Q_H}$$

If  $Q_L \neq 0$ , then,  
 $\eta$  is always less than 1



$$COP_R = \frac{Q_L}{Q_H - Q_L}$$

$$COP_{HP} = \frac{Q_H}{Q_H - Q_L}$$

Since,  $Q_H \neq Q_L$ , so COP will  
 never be  $\infty$ .

WHAT IS THE MAXIMUM POSSIBLE EFFICIENCY?  
 HOW CAN WE GUARANTEE MAXIMUM POSSIBLE EFFICIENCY?

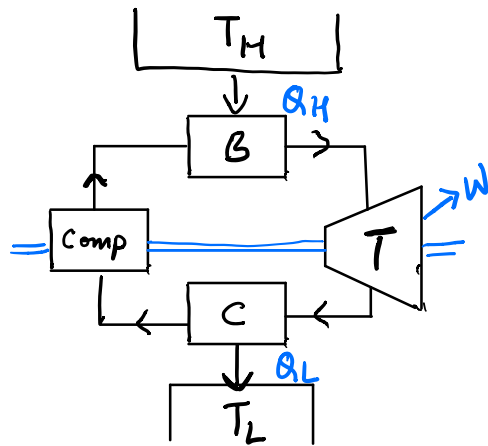
### REVERSIBLE PROCESS

We make a cycle reversible by avoiding irreversible processes.

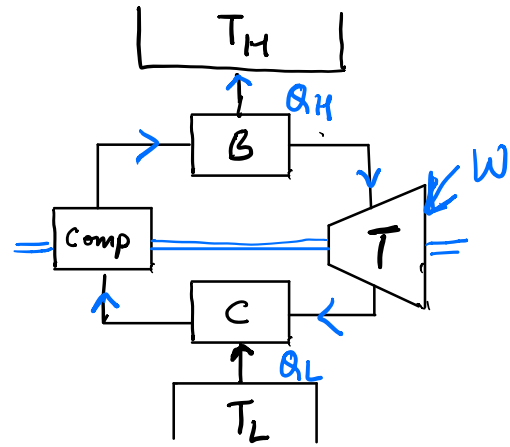
- friction
- unconstrained expansion
- mixing
- heat transfer
- chemical rxn

To create an engine that





Forward Carnot Cycle  
(HE Carnot Cycle)



Reversed Carnot Cycle  
(REF Carnot Cycle)

For Reversible cycles

$$\frac{Q_2}{Q_1} = \frac{T_2}{T_1}$$



6-28 A coal-burning steam power plant produces a net power of 300 MW with an overall thermal efficiency of 32 percent. The actual gravimetric air-fuel ratio in the furnace is calculated to be 12 kg air/kg fuel. The heating value of the coal is 28,000 kJ/kg. Determine (a) the amount of coal consumed during a 24-hour period and (b) the rate of air flowing through the furnace. Answers: (a)  $2.89 \times 10^6$  kg, (b) 402 kg/s

Here, steam-power plant  $\Rightarrow$  heat engine

$$\dot{W}_{\text{net,out}} = 300 \text{ MW} = 300 \times 10^6 \text{ W}$$

$$\eta_t = 0.32$$

$$\eta_t = \frac{\dot{W}_{\text{net,out}}}{\dot{Q}_{\text{in}}} \Rightarrow \dot{Q}_{\text{in}} = \frac{300}{0.32} = 937.5 \text{ MW}$$

$$\therefore Q_{\text{in}} = \dot{Q}_{\text{in}} \Delta t = 937.5 \times (24 \times 3600) = 8.1 \times 10^7 \text{ MJ}$$

$$m_{\text{coal}} = \frac{Q_{\text{in}}}{q} = \frac{8.1 \times 10^7}{28} = 2.893 \times 10^6$$

An irreversible heat engine extracts heat from a high temperature source at a rate of 100 kW and rejects heat to a sink at a rate of 50 kW. The entire work output of the heat engine is used to drive a reversible heat pump operating between a set of independent isothermal heat reservoirs at 17°C and 75°C. The rate (in kW) at which the heat pump delivers heat to its high temperature sink is

A] 50

B] 25

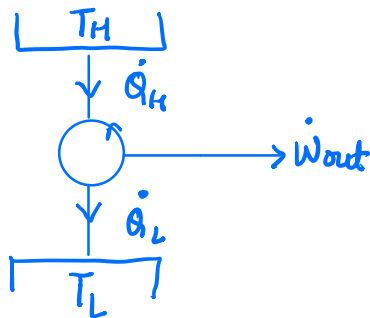
C] 300

D] 360

HINT:  $\frac{Q_H}{Q_L} = \frac{T_H}{T_L}$  , for reversible process

Here,

For irreversible H.E

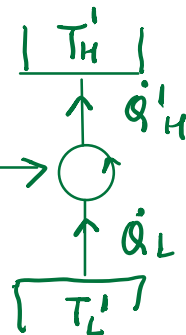


$$\dot{Q}_H = 100 \text{ kW}$$

$$\dot{Q}_L = 50 \text{ kW}$$

$$\dot{W}_{out} = \dot{Q}_H - \dot{Q}_L$$

For reversible H.P.



$$T'_L = 17^\circ\text{C} = 290 \text{ K}$$

$$T'_H = 75^\circ\text{C} = 348 \text{ K}$$

$$\text{COP} = \frac{T'_H}{T'_L}$$



$$= 100 - 50$$

$$= 50 \text{ KW}$$

$$\frac{T_H' - T_L'}{348 - 290}$$

$$= 6$$

$$\text{But, COP} = \frac{\dot{Q}_H}{\dot{W}_{\text{out}}}$$

$$\text{or } \dot{Q}_H = \text{COP} (\dot{W}_{\text{out}})$$

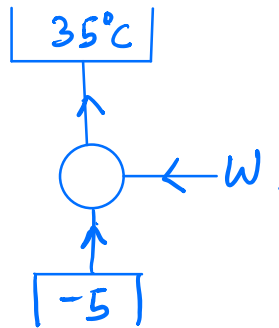
$$= 6 (50)$$

$$= 300 \text{ KW}$$

$\therefore$  300 KW is supplied to the high temperature reservoir of the heat pump.

A reversed Carnot cycle refrigerator maintains a temp of  $-5^{\circ}\text{C}$ . The ambient air temperature is  $35^{\circ}\text{C}$ . The heat gained by the refrigerator at a continuous rate is  $2.5 \text{ kJ/s}$ . The power (in watt) required to pump this heat out continuously is \_\_\_\_\_?

Here,



$$T_L = -5 = 268 \text{ K}$$

$$T_H = 35 = 308 \text{ K}$$

$$\text{COP} = \frac{T_L}{T_H - T_L} = \frac{268}{308 - 268} = 6.7$$

Also,

$$\text{COP} = \frac{\dot{Q}_L}{\dot{W}}$$

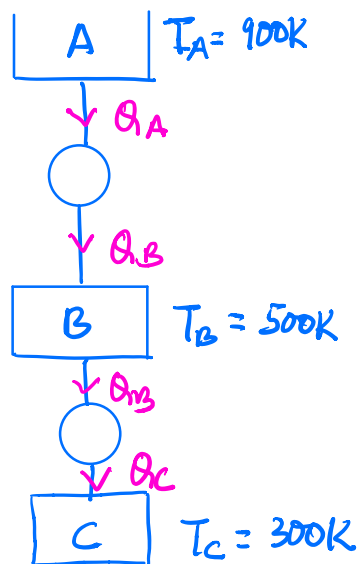
$$\Rightarrow \dot{W} = \frac{\dot{Q}_L}{\text{COP}} = \frac{2500}{6.7} = 373.134 \text{ W}$$



Carnot engine (CE-1) works between two temperature reservoirs A and B, where  $T_A = 900\text{K}$  and  $T_B = 500\text{K}$ . A second Carnot engine (CE-2) works between temperature reservoir B and C, where  $T_C = 300\text{K}$ .

In each cycle of CE-1 and CE-2, all the heat rejected by CE-1 to reservoir B is used by CE-2. For one cycle of operation, if net  $Q$  absorbed by CE-1 from reservoir A is  $150\text{MJ}$ , the net heat rejected to reservoir C by CE-2 (in MJ) is \_\_\_\_\_?

- A]  $100\text{MJ}$       B]  $50\text{MJ}$       C]  $75\text{MJ}$       D]  $25\text{MJ}$



$$\eta_1 = 1 - \frac{500}{900} = 1 - \frac{Q_B}{150}$$

$$\Rightarrow Q_B = 83.33\text{ MJ}$$

$$1 - \frac{300}{500} = 1 - \frac{Q_C}{83.33}$$

$$Q_C = 50\text{ MJ}$$